THE OPTIMIZATION OF ULTRASOUND-ASSISTED EXTRACTION OF TOTAL FLAVONOIDS FROM POT MARIGOLD
(*Calendulae officinalis* L.) FLOWERS

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Pot marigold (*Calendula officinalis* L.) contains various bioactive compounds such as flavonoids, tannins, saponosides, carotenoids, triterpene alcohols, polysaccharides, amino acids, and essential oil. The extract of pot marigold flower has a benefit to the skin due to the presence of flavonoids that possess the anti-inflammatory, astringent, antifungal, and antiseptic effects. The aim of this study was to apply the ultrasound-assisted extraction as an advanced extraction technique and to investigate the impact of extraction time (5-35 min), ethanol concentration (20-80%, v/v), and extraction temperature (30-70 °C) on the total flavonoid content of pot marigold flower at the liquid-to-solid ratio of 20 cm$^3$ g$^{-1}$. The total flavonoids content of the extracts was determined spectrophotometrically with aluminium (III) chloride. The modeling of ultrasound-assisted extraction was carried out using a Box-Behnken design. Thus found optimal extraction conditions were the extraction time of 29 min, 39.6% (v/v) ethanol, and extraction temperature of 64.2 °C. The experimental value (220.2 mg 100 g$^{-1}$ d.w.) of the total flavonoid content under optimal conditions was in a good agreement with the predicted value (221.5 mg 100 g$^{-1}$ d.w.). According to the results of statistical analysis, the proposed second-order polynomial equation can be used to describe the extraction of flavonoids and to predict the total flavonoid content. The extraction procedure can be accepted from the point of the pharmaceutical application due to the use of ethanol as a representative of green solvents. The extraction time was shorter compared with other conventional extraction techniques.

**Keywords:** ultrasound-assisted extraction, flavonoids, *Calendulae officinalis*, Box-Beihnenk.

**Introduction**

Pot marigold (*Calendula officinalis* L.) originates from the Mediterranean [1], and grows in the gardens and parks of Central and Southern Europe, Western Asia and USA [2]. It reaches a height between 30 and 60 cm [2,3]. Its flower has yellow or orange colour and a unique fragrance [3]. Therapeutic properties of the flower are attributed to various types of bioactive compounds, such as: flavonoids, tannins, saponosides, carotenoids, triterpene alcohols, polysaccharides, amino acids, and essential oils [2, 4-6]. The extract of pot marigold flower has the antioxidant [7-12], antimicrobial [13-15], anti-inflammatory [16,17], anticancer [18,19], spasmyloytic [20], hepatoprotective, and rheumatic protective activities [21]. Due to the complex chemical content and broad spectrum of pharmacological activity, this plant material has an application in pharmaceutical and cosmetic industries. The pot marigold is described in German and the Russian Pharmacopoeia, as well as in the supplement of European Pharmacopoeia 6.0 [22], but is not described by Yugoslavian Pharmacopoeia V [23]. In folk medicine, it is used as a mild antiseptic for outdoor and indoor use in the form of tea, tincture, and ointment. Tea is effective in the treatment of inflammation of the gastro-system, bile, hemorrhoids, veins, and capillaries. It causes sweating, cleans the liver, restores the viscosity of the blood, calms the open wounds, stains, mites, and aging spots [24]. In the official medicine, it is used for the symptomatic treatment of mild skin inflammations (burns from the sun), minor wounds and inflammation of the oral cavity [25].

The hydrodistillation of the essential oil from fresh flowers of pot marigold have been described in British Pharmacopoeia [26], while the preparation of its tincture with 40% (v/v) and 60% (v/v) ethanol was proposed in European Pharmacopoeia [27]. Matysik et al. [28] quantified flavonoids and pentacyclic triterpene in methanol, ethyl acetate and heptane extracts using a chromatographic method. The extracts were prepared by reflux extraction at the temperature of 60 °C for 5 h. Bakó et al. [6] prepared the methanolic extract by maceration in order to identify carotenoids in the plant material. The plant material was treated by the solvent at room temperature for 20 h. The ethanolic extract obtained using maceration was used to analyze the hepatoprotective functions of the pot marigold extract [21].

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The manuscript received: April, 06, 2019.
The thin-layer chromatographic method was used to identify bioactive compounds and estimate the pharmacological activity of the n-hexane and methanolic extracts obtained using Soxhlet extraction at 70 °C for 8 h [29]. The ethanolic and methanolic extracts obtained at 35 °C for 24 h were subjected to define their antimicrobial activity [14]. Recently, the main effort in many studies was focused in the direction of the development of the advanced extraction techniques that are more superior to other available conventional methods. A supercritical carbon dioxide extraction technique is one of them used for the preparation of the pot marigold extract [11,30] and for obtaining the essential oil [31]. The ultrasound-assisted extraction as an advanced extraction technique provides the higher extraction yield of about 34% compared to the conventional extraction technique [32]. García-Risco et al. [11] confirmed that the extract obtained by using 50% (v/v) ethanol and the ultrasound-assisted extraction has a higher phenolic content than the extract prepared by using pure ethanol.

The ultrasound-assisted extraction represents the technique of choice for the extraction of flavonoids from pot marigold. The simultaneous impact of different parameters on the yield of flavonoids has not been reported yet in the literature so that the aim of this paper was to investigate the impact of the extraction time, ethanol concentration, and extraction temperature on the total flavonoid content (TFC) of pot marigold. The TFC was determined using a spectrophotometric method with aluminium(III) chloride. Box-Behnken design was employed to model the extraction procedure and to define the interactions between investigated extraction parameters. The application of the design reduced the number of experimental runs needed for optimization compared to the one-variable-at-a-time method.

**Experimental**

**Materials**

Chemicals and reagents

Rutin trihydrate (purity of 97%) (Alfa Aesar - Johnson Matthey Company, Heysham, Great Britain), methanol, 96% ethanol (Zorka Pharma, Sabac, Republic of Serbia), aluminium(III) chloride, potassium acetate (Sigma Chemical, Saint Louis, Missouri, USA) were used.

**Plant material**

Pot marigold (Calendulae officinalis L.) flowers were purchased from “Josif Pančić” (Belgrade, Republic of Serbia). The moisture content of 14.4% (w/w) was determined by drying of the plant material in a laboratory oven at 105 °C until the constant mass.

**Methods**

**Extraction procedure of pot marigold flowers**

The extractions assisted by ultrasound were performed in an ultrasonic bath (Sonic, Niš, Republic of Serbia). The used frequency was 40 kHz, while the power was 150 W. The liquid-to-solid ratio was 20 cm³ g⁻¹. After extraction, the plant material was separated by filtration under vacuum. The extract was evaporated under vacuum at 50 °C and stored in a desiccator before further analysis.

**Box-Behnken design**

The three extraction parameters (extraction time, ethanol concentration, and extraction temperature) were varied at three levels (-1, 0, +1) according to the Box-Behnken design, representing an alternative to a central composite design. The design which represents a combination of a fractional factorial design and an incomplete block design [33] is suitable for optimization of the extraction process [34]. The TFC was defined as a design response.

According to Equation 1, the actual factors ($x_i$) were converted to coded for better uniformity [33].

$$x_{i}^{c} = \frac{x_{i} - X_{i}}{\Delta x_{i}}$$

where $x_i -$ coded value of factor, $x_i -$ actual value of factor, $X_i -$ actual value in the center point, $\Delta x_i -$ the step change of value. In Table 1, the levels of the analyzed factors are depicted.

<table>
<thead>
<tr>
<th>Factors</th>
<th>actual</th>
<th>coded</th>
<th>Factor levels</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>1</td>
<td>0</td>
<td>+1</td>
</tr>
<tr>
<td>Extraction time [min]</td>
<td>$x_1$</td>
<td>$X_1^c$</td>
<td>5</td>
</tr>
<tr>
<td>Ethanol concentration [% (v/v)]</td>
<td>$x_2$</td>
<td>$X_2^c$</td>
<td>20</td>
</tr>
<tr>
<td>Extraction temperature [°C]</td>
<td>$x_3$</td>
<td>$X_3^c$</td>
<td>30</td>
</tr>
</tbody>
</table>

The TFC of pot marigold was determined according to a standard procedure with aluminium(III) chloride [35].

The 17 extractions were performed in order to apply this design for modeling of the extraction process. The extraction of flavonoids was described using a second-order polynomial equation (Equation 2) [34]:

$$Y = a_0 + a_1x_1 + a_2x_2 + a_3x_3 + a_{12}x_1x_2 + a_{13}x_1x_3 + a_{23}x_2x_3 + a_{11}x_1^2 + a_{22}x_2^2 + a_{33}x_3^2 + \varepsilon$$

where $Y -$ system response (TFC); $x_1$, $x_2$, $x_3 -$ factors; $a_{ij} -$ intercept; $a_1, a_2, a_3, a_{12}, a_{13}, a_{23}, a_{11}, a_{22}, a_{33} -$ regression coefficients, and $\varepsilon -$ residual. The parameter $\varepsilon$ represents the model error (lack-of-fit) and the experimental error (pure error).

The coefficients of the polynomial equation were determined using the method of the least squares. Design Expert 11.0.3.0 (Stat-Ease, Minneapolis, Minnesota, USA) was used for a statistical analysis of the proposed regression model. The effect of analyzed factors was estimated based on the analysis of variance (ANOVA).

The terms in the polynomial equation were analyzed and statistically verified using F-test with a 95% confidence interval (p<0.05). Based on the coefficient of determination, the adequacy of model was confirmed.

Determination of total flavonoid content

The TFC of pot marigold was determined according to a standard procedure with aluminium(III) chloride [35].
The content was expressed as milligram rutin equivalent per 100 g of the dry weight (mg\textsubscript{RE} 100 g\textsuperscript{-1} d.w.). The stock solution of rutin (1.0 mg cm\textsuperscript{-3}) in methanol was used to prepare a series of solutions in the concentration range of 1-100 μg cm\textsuperscript{-3}. The sample consisted of 2.0 cm\textsuperscript{3} of a methanolic solution of rutin (or the extract), 0.1 cm\textsuperscript{3} of aluminium(III)-chloride (10%, w/w), 0.1 cm\textsuperscript{3} of potassium acetate (1 mol dm\textsuperscript{-3}), and 2.8 cm\textsuperscript{3} of distilled water. Instead of aluminium(III) chloride, a blank solution contained the equivalent amount of distilled water. Varian Cary-100 Conc (Mulgrave, Victoria, Australia) spectrophotometer was employed to measure the absorbance of the samples at 415 nm in a quartz cuvette of 1×1 cm at room temperature (22 °C).

Results and discussion

Modeling the extraction procedure

The content of the extract depends on the used solvent and the extraction method [36]. Green solvents have the advantage for the extraction of bioactive compounds from plant materials compared with other solvents since the obtained extract can be used in food, pharmaceutical, and cosmetic industries [37]. Among them, ethanol is commonly used as a solvent due to its properties, such as non-toxicity and eco-friendly to obtain the extract of the desired content. Since the flavonoid content depends on the solvent polarity [38], the impact of different ethanol concentrations was analyzed in this study. The calibration curve of rutin (Equation 3) was used to determine the TFC in the extracts:

\[ A_{415} = 14.2C_{R} + 0.05 \]  \hspace{1cm} \left( R^{2} = 0.999 \right)

where \( A_{415} \) – absorbance at 415 nm expressed in AU, \( C_{R} \) – concentration of rutin expressed in mg cm\textsuperscript{-3}. Linearity of the calibration curve was noticed in the concentration range of 5-100 μg cm\textsuperscript{-3}.

Before the optimization using Box-Behnken design, the statistically significant factors (extraction time, ethanol concentration, and extraction temperature) were confirmed using a screening design. According to a matrix of Box-Behnken design presented in Table 2, the factors were varied as presented. In addition to the random order of extractions representing the combination of different factor levels, the experimental and predicted values of TFC are also given. The experimental TFC values were in the range between 114.7 and 221.0 mg\textsubscript{RE} 100 g\textsuperscript{-1} d.w., so that flavonoids are approximately 0.2% of the dry plant material.

![Table 2](https://example.com/table2.png)

The TFC was fitted using the second-order polynomial model containing linear and quadratic terms. The model and coefficients of the equation were obtained by statistical non-linear regression of experimental data. The polynomial model establishes the relationship between the factors and the response. The most acceptable model is defined by the highest coefficient of correlation (R) and the coefficient of determination (R\textsuperscript{2}). In an ideal case, these values are 1, indicating a good agreement between the experimental and predicted values [39]. The
regression coefficients of the polynomial equation with the coded and actual factors, as well as the coefficients of determination are given in Table 3. The equation in terms of actual factors is used for the prediction of the response and is not used when determining the relative effect of each individual factor. For this reason, the importance of each term was estimated based on the regression coefficients in the equations with coded factors. The positive regression coefficient indicates a positive impact on the TFC in the extracts and vice versa. The analysis of linear effects in the equation indicated that the ethanol concentration had a negative impact on the TFC [40]. The highest impact had the extraction time and then follows the extraction temperature and the ethanol concentration.

### Table 3. The regression coefficients of the second-order polynomial equation with coded and actual values of factors

<table>
<thead>
<tr>
<th>Factor</th>
<th>Coded factor</th>
<th>Actual factor</th>
</tr>
</thead>
<tbody>
<tr>
<td>Intercept</td>
<td>201.98</td>
<td>-32.30</td>
</tr>
<tr>
<td>A-extraction time</td>
<td>24.39</td>
<td>6.73</td>
</tr>
<tr>
<td>B-ethanol conc.</td>
<td>-13.97</td>
<td>4.09</td>
</tr>
<tr>
<td>C-extraction temp.</td>
<td>17.1</td>
<td>1.55</td>
</tr>
<tr>
<td>AB</td>
<td>-18.95</td>
<td>-0.04</td>
</tr>
<tr>
<td>AC</td>
<td>2.16</td>
<td>0.01</td>
</tr>
<tr>
<td>BC</td>
<td>8.82</td>
<td>0.01</td>
</tr>
<tr>
<td>A²</td>
<td>-18.89</td>
<td>-0.08</td>
</tr>
<tr>
<td>B²</td>
<td>-40.05</td>
<td>-0.04</td>
</tr>
<tr>
<td>C²</td>
<td>-6.28</td>
<td>-0.02</td>
</tr>
</tbody>
</table>

### Table 3. The regression coefficients of the second-order polynomial equation with coded and actual values of factors

<table>
<thead>
<tr>
<th></th>
<th>Sum of squares</th>
<th>Degrees of freedom</th>
<th>Mean squares</th>
<th>F-value</th>
<th>p-value</th>
</tr>
</thead>
<tbody>
<tr>
<td>Model</td>
<td>19429.25</td>
<td>9</td>
<td>2158.81</td>
<td>40.20</td>
<td>&lt; 0.0001*</td>
</tr>
<tr>
<td>X₁</td>
<td>4760.44</td>
<td>1</td>
<td>4760.44</td>
<td>88.64</td>
<td>&lt; 0.0001*</td>
</tr>
<tr>
<td>X₂</td>
<td>1560.76</td>
<td>1</td>
<td>1560.76</td>
<td>29.06</td>
<td>0.001*</td>
</tr>
<tr>
<td>X₃</td>
<td>2338.50</td>
<td>1</td>
<td>2338.50</td>
<td>43.55</td>
<td>0.0003*</td>
</tr>
<tr>
<td>X₁X₂</td>
<td>1436.89</td>
<td>1</td>
<td>1436.89</td>
<td>26.76</td>
<td>0.0013*</td>
</tr>
<tr>
<td>X₁X₃</td>
<td>18.64</td>
<td>1</td>
<td>18.64</td>
<td>0.35</td>
<td>0.5743*</td>
</tr>
<tr>
<td>X₂X₃</td>
<td>310.98</td>
<td>1</td>
<td>310.98</td>
<td>5.79</td>
<td>0.0470*</td>
</tr>
<tr>
<td>X₁²</td>
<td>1502.51</td>
<td>1</td>
<td>1502.51</td>
<td>27.98</td>
<td>0.0011*</td>
</tr>
<tr>
<td>X₂²</td>
<td>6754.50</td>
<td>1</td>
<td>6754.50</td>
<td>125.78</td>
<td>&lt; 0.0001*</td>
</tr>
<tr>
<td>X₃²</td>
<td>166.18</td>
<td>1</td>
<td>166.18</td>
<td>3.09</td>
<td>0.1220*</td>
</tr>
<tr>
<td>Residual</td>
<td>375.92</td>
<td>7</td>
<td>53.70</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Lack-of-fit</td>
<td>196.20</td>
<td>3</td>
<td>65.40</td>
<td>1.46</td>
<td>0.3525*</td>
</tr>
<tr>
<td>Pure error</td>
<td>179.72</td>
<td>4</td>
<td>44.93</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Cor. total</td>
<td>19805.17</td>
<td>16</td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Std. dev.</td>
<td>7.33</td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Mean</td>
<td>171.29</td>
<td>R²</td>
<td>0.981</td>
<td></td>
<td></td>
</tr>
<tr>
<td>C.V. %</td>
<td>4.28</td>
<td>R²adj</td>
<td>0.957</td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

*R*-statistically significant; **-statistically insignificant
The coefficient of determination of 0.981 indicated that a 1.9% variation in the TFC could not be explained by the regression model. The predicted coefficient of determination (0.827) was in good agreement with the adjusted coefficient of determination (0.957), given that the difference between these two values was less than 0.2 [41]. A detail statistical analysis was carried out in order to confirm the reliability of the chosen model. ANOVA of the proposed model is given in Table 4. The model F-value of 40.2 implied that the regression model was statistically significant. The lack-of-fit was not statistically significant comparing to pure error (179.72), because its F-value of 1.46 was lower than the critical value of 6.59. The statistically insignificant lack-of-fit indicated that the proposed model was adequate for the prediction of response. The adequate precision of 19.00 implied a good signal-to-noise ratio. Since this value was higher than the limited value of 4 [42], the model can be used to navigate the design space.

The p-value for statistically significant terms was lower than 0.05 [42]. Not statistically significant terms in the polynomial equation were the interaction between the extraction time and the extraction temperature, as well as the quadratic effect of the extraction temperature. In order to improve the regression model, these terms can be excluded from the proposed polynomial equation.

Since the data follow the linearity in the normal probability plot of studentized residuals presented in Figure 1, it can be concluded that the residuals have normal distribution [34]. The analysis of Cook’s distances (Table 2) indicated that there were no significant points (outliers) because all values of TFC were lower than the critical value of 1.0.

![Figure 1. Normal probability plot of studentized residuals.](image)

The three-dimensional plots were a suitable graphical method to investigate the interactions between factors and their impact on the TFC. In Figure 2, the impact of the extraction time and the ethanol concentration at the extraction temperature of 50 °C is depicted. The surface shape indicated a strong interaction between analyzed factors. The increase of the extraction time leads to the increase of TFC which is more expressed for shorter than 15 min. This was expected because of the rapid period of extraction which occurs in the first extraction time. Using this extraction technique, the increase of mass transfer velocity and destroyed plant cells are possible to achieve after the effect of cavitation energy [43]. The effect of the extraction time was more significant at lower ethanol concentrations (<50%, v/v).

![Figure 2. The impact of the extraction time and the ethanol concentration on the total flavonoid content at the extraction temperature of 50 °C.](image)

In Figure 3, the interaction between the ethanol concentration and the extraction temperature for the extraction time of 20 min is presented. The increase of the ethanol concentration especially above 50% (v/v) leads to a decrease of TFC in the extracts. After the analysis of the diagram, it can be concluded that the extraction temperature has a positive impact on the TFC. The diffusion increases not only because of the increase of the extraction temperature but also due to improved hydrodynamic conditions [44]. Namely, the viscosity of the solvent decreases with increasing the temperature, which increases the penetration rate in the plant material, and consequently the concentration of flavonoids in the extract [45].

The impact of the extraction time and the extraction temperature on the TFC using 50% (v/v) ethanol is depicted in Figure 4. It is clearly observed that the TFC was increased with increasing the extraction temperature for the same extraction time. This effect is more pronounced at longer extraction times (>20 min). The extraction time
influences positively on the TFC at the constant extraction temperature; it can be clearly seen that this factor has a positive effect on the TFC.

Figure 3. The impact of the ethanol concentration and the extraction temperature on the total flavonoid content for the extraction time of 20 min.

Figure 4. The impact of the extraction time and the extraction temperature on the total flavonoid content using 50% (v/v) ethanol.

Optimization of the extraction procedure

Numerical optimization method was used to obtain the optimal extraction conditions. The TFC was maximized and the following conditions were obtained: the extraction time of 29 min, the ethanol concentration of approximately 40% (v/v), and the extraction temperature of approximately 64 °C (Figure 5) at the liquid-to-solid ratio of 20 cm$^3$ g$^{-1}$. Under these conditions, the regression model predicts the TFC of 221.5 mg 100 g$^{-1}$ d.w., while the experimental value is 220.2 mg 100 g$^{-1}$ d.w.

The extraction under optimal conditions was performed to estimate the prediction ability of the proposed model. A good agreement between these two values indicates the adequate prediction ability.

Figure 5. The optimal conditions of the flavonoid extraction from pot marigold flowers.

The TFC depends on the extraction techniques, solvents, and used procedures for its determination. The extract of pot marigold prepared by maceration using 70% (v/v) ethanol has the TFC of 1.45% [1]. Jurca et al. [12] defined the TFC as milligram quercetin equivalent per 100 g of the dry weight (mg$_{eq}$ 100 g$^{-1}$ d.w.). In the lyophilized and alcoholic extracts obtained by maceration with 95% (v/v) ethanol at 20 °C for 72 h, the TFC was 266.62 mg$_{eq}$ 100 g$^{-1}$ d.w. and 42.12 mg$_{eq}$ 100 g$^{-1}$ d.w., respectively [12]. Bilia et al. [46,47] determined the TFC of 58.4 mg 100 cm$^3$ and 57.1 mg 100 cm$^3$ in the tinctures prepared using 40% (v/v) i 60% (v/v) ethanol, respectively. García-Risco et al. [11] reported that the extract obtained by ultrasound-assisted extraction with 50% (v/v) ethanol has the highest TFC of 50 mg$_{eq}$ g$^{-1}$ of the extract compared with the extracts obtained by ultrasound-assisted extraction (25 mg$_{eq}$ g$^{-1}$ of the extract) with absolute ethanol and by supercritical fluid extraction (>25 mg$_{eq}$ g$^{-1}$ of the extract).

Conclusion

The extraction of flavonoids from pot marigold flowers assisted by ultrasound was described using the second-order polynomial equation. Box-Behnken design was successfully applied for the optimization of the extraction process. The impact of three factors: extraction time, ethanol concentration, and extraction temperature on the TFC was analyzed at the liquid-to-solid ratio of 20 cm$^3$ g$^{-1}$. The extraction time had the highest impact, while the extraction temperature and the ethanol concentration had a slightly lower impact. The linear effect of the ethanol concentration has a negative impact on the content of TFC in the extract. The optimal conditions: extraction time of 29 min, ~40% (v/v) ethanol, and approximately extraction temperature of 64 °C were obtained after the application of the numerical optimization method. The experimental (220.2 mg 100 g$^{-1}$ d.w.) and predicted (221.5 mg 100 g$^{-1}$ d.w.) values under optimal conditions, as well as the coefficients of determination were in good agreement. The adequate precision of 19 was higher than the required minimum of 4. This value indicated the adequate signal-to-noise ratio of this model. Based
on these facts, the proposed model can be used for the prediction of TFC in the design space. The proposed procedure for the extraction of flavonoids is acceptable for the application in the pharmaceutical industry due to the use of ethanol as a green solvent. The ultrasound-assisted extraction was an efficient advanced extraction technique because time for the extraction of flavonoids was reduced.

Acknowledgment

The authors acknowledge the financial support for this study from the Ministry of Education, Science and Technological Development of the Republic of Serbia by Grant No. TR-34012.

References


POSTUPAK EKSTRAKCIJE UKUPNIH FLAVONOIDA IZ CVETA NEVENA 
(Calendulae officinalis L.)

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Neven (Calendula officinalis L.) sadrži različita bioaktivna jedinjenja, kao što su: flavonoidi, tanini, saponozidi, karotenoidi, triterpenski alkoholi, polisaharidi, aminokiseline i etarsko ulje. Ekstrakt cveta nevena blagotvorno deluje na kožu usled prisustva flavonoida koji imaju antiinflamatorno, adstringentno, antifungalno i antiseptično dejstvo. Cilj rada bio je da se primeni ultrazvučna ekstrakcija kao savremena tehnika i da se ispita uticaj vremena ekstrakcije (5-35 min), koncentracije etanola (20-80%, v/v) i temperature ekstrakcije (30-70 °C) na sadržaj ukupnih flavonoida cveta nevena pri odnosu rastvarača i biljne sirove od 20 cm$^3$ g$^{-1}$. Sadržaj ukupnih flavonoida ekstrakata određen je spektrofotometrijski sa aluminijum(III) hloridom. Modelovanje ultrazvučne ekstrakcije izvršeno je primenom Box-Behnkenovog dizajna. Tako dobijeni optimalni uslovi bili su: vreme ekstrakcije od 29 min, 39,6% (v/v) etanol i temperatura ekstrakcije od 64,2 °C. Eksperimentalna vrednost (220,2 mg 100 g$^{-1}$ s.m.) sadržaja ukupnih flavonoida pri optimalnim uslovima bila je u dobroj saglasnosti sa predviđenom vrednošću (221,5 mg 100 g$^{-1}$ s.m.). Prema rezultatima statističke analize, predložena polinomna jednačina drugog reda može se upotreti da opiše ekstrakciju flavonoida i da predvidi sadržaj ukupnih flavonoida. Postupak ekstrakcije može se prihvatiti sa stanovišta farmaceutske primene usled primene etanola kao predstavnika zelenih rastvarača. Vreme ekstrakcije bilo je kraće u poređenju sa drugim konvencionalnim tehnikama ekstrakcije.